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**UTILITY
PATENT APPLICATION
TRANSMITTAL**

(Only for new nonprovisional applications under 37 CFR 1.53(b))

Attorney Docket No. OKL 0120 PUS

First Inventor Eli Oklejas, Jr.

Title Method and Apparatus for Membrane Recirculation and Concentrate Energy Recovery in a Reverse Osmosis System

Express Mail Label No. EL596484726US

APPLICATION ELEMENTS

See MPEP chapter 600 concerning utility patent application contents.

1. ☒ Fee Transmittal Form (e.g., PTO/SB/17)
(Submit an original and a duplicate for fee processing)
2. ☒ Applicant claims small entity status.
See 37 CFR 1.27.
3. ☒ Specification [Total Pages]
(preferred arrangement set forth below)
- Descriptive title of the invention
 - Cross Reference to Related Applications
 - Statement Regarding Fed sponsored R & D
 - Reference to sequence listing, a table, or a computer program listing appendix
 - Background of the Invention
 - Brief Summary of the Invention
 - Brief Description of the Drawings (if filed)
 - Detailed Description
 - Claim(s)
 - Abstract of the Disclosure
4. ☒ Drawing(s) (35 U.S.C. 113) [Total Sheets]
5. Oath or Declaration [Total Pages]
- a. ☒ Newly executed (original or copy)
Copy from a prior application (37 CFR 1.63 (d))
(for continuation/divisional with Box 17 completed)
- b. ☐ **DELETION OF INVENTOR(S)**
Signed statement attached deleting inventor(s)
named in the prior application, see 37 CFR
1.63(d)(2) and 1.33(b).
6. ☐ Application Data Sheet. See 37 CFR 1.76

ADDRESS TO: Assistant Commissioner for Patents
Box Patent Application
Washington, DC 20231

7. ☐ CD-ROM or CD-R in duplicate, large table or
Computer Program (Appendix)
8. Nucleotide and/or Amino Acid Sequence Submission
(if applicable, all necessary)
- a. ☐ Computer Readable Form (CRF)
- b. Specification Sequence Listing on:
- i. ☐ CD-ROM or CD-R (2 copies); or
 - ii. ☐ paper
- c. ☐ Statements verifying identity of above copies

ACCOMPANYING APPLICATION PARTS

9. ☐ Assignment Papers (cover sheet & document(s))
10. ☐ 37 CFR 3.73(b) Statement ☒ Power of Attorney
(when there is an assignee)
11. ☐ English Translation Document (if applicable)
12. ☒ Information Disclosure ☒ Copies of IDS
Statement (IDS)/PTO-1449 Citations
13. ☐ Preliminary Amendment
14. ☒ Return Receipt Postcard (MPEP 503)
(Should be specifically itemized)
15. ☐ Certified Copy of Priority Document(s)
(if foreign priority is claimed)
16. ☒ Other: Check

17. If a CONTINUING APPLICATION, check appropriate box, and supply the requisite information below and in a preliminary amendment, or in an Application Data Sheet under 37 CFR 1.76:

☐ Continuation ☐ Divisional ☐ Continuation-in-part (CIP)

of prior application No. _____ / _____

Prior application information:

Examiner _____

Group / Art Unit. _____

For CONTINUATION OR DIVISIONAL APPS only: The entire disclosure of the prior application, from which an oath or declaration is supplied under Box 5b, is considered a part of the disclosure of the accompanying continuation or divisional application and is hereby incorporated by reference. The incorporation can only be relied upon when a portion has been inadvertently omitted from the submitted application parts.

18. CORRESPONDENCE ADDRESS☐ Customer Number or Bar Code Label

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**METHOD AND APPARATUS FOR MEMBRANE
RECIRCULATION AND CONCENTRATE ENERGY RECOVERY
IN A REVERSE OSMOSIS SYSTEM**

Related Applications

The present application relates to U.S. Patent Application 09/491,769 entitled "Hydraulic Energy Recovery Device" filed January 26, 2000, and U.S. Patent Application (Attorney Docket No OKL-
5 0118PA) entitled "Method And Apparatus for Boosting Interstage Pressure In A Reverse Osmosis System", each of which are hereby incorporated by reference.

Technical Field

The present invention relates generally to a reverse osmosis systems suitable for desalinization
10 of water, and more specifically, to a recirculation system and concentrate energy recovery in a reverse osmosis system.

Background of the Invention

Reverse osmosis (RO) is a process widely used for desalinization of water. Reverse osmosis
15 membranes are contained in a process chamber into which pressurized feedwater is admitted. A portion of the pressurized water permeates across the membrane and exits the process chamber as purified water at a low pressure and is referred to as
20 permeate. The remainder of the water, still at high pressure, exits the process chamber and is referred to as a concentrate.

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about 30 psi in the present example. Thus, feed pump 12 must pressurize the recirculation flow as well as the feed flow.

Another known arrangement similar to Figure 1 is illustrated having the same components illustrated with the same reference numerals. In this embodiment, a pump 30 driven by a motor 32 couples concentrate at an elevated pressure above that of the feed stream.

One problem with these types of systems is that although they are more energy efficient than other known systems, energy dissipated in control valve 28 cannot be recovered. Another drawback to this type of system is that recirculation pump 30 is expensive because of the high working pressure. Another drawback to the system is that the motor 32 consumes a substantial amount of energy.

Summary of the Invention

It is therefore one object of the invention to provide a reverse osmosis system that uses concentrate recirculation to allow the membrane to operate efficiently while recovering otherwise wasted energy.

In one aspect of the invention a process chamber preferably a reverse osmosis chamber, has a feed inlet, a low pressure outlet, and a high pressure outlet. A feed pump is used to increase the pressure of feed fluid to feed inlet.

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A common shaft is used to rotatably couple a booster and an energy recovery turbine together. The energy recovery turbine is fluidically coupled to the high pressure outlet to drive the booster pump.
5 The booster pump is positioned between the feed pump and process chamber and increases the pressure of feed fluid.

In a further aspect of the invention, a method for operating a reverse osmosis system
10 comprises the steps of:

boosting a pressure of fluid output from a feed pump prior to entering to a first process chamber using from a first portion of a high pressure fluid from a high pressure outlet of a first process
15 chamber;

recirculating a second portion of the high pressure fluid; and

fluidically coupling the second portion of the high pressure fluid between the feed pump and the
20 process chamber.

One advantage of the present invention is that energy-wasting throttle valves and bypass lines have been eliminated from the reverse osmosis process. Another advantage of the invention is that
25 more energy is recovered from the process lowering the overall cost of operating such a process. Another advantage is that the components can be combined into a single package.

Other objects and features of the present
30 invention will become apparent when viewed in light

Detailed Description of the Preferred Embodiment

In the following figures, the same references numerals will be used to identify identical components in the various views.

5 The present invention is described with respect to various preferred embodiments and preferred system uses. One skilled in the art would recognize various alternatives without varying from the spirit of the invention such as non-desalinization reverse osmosis systems.

10 Referring now to Figure 3, an improved embodiment similar to that shown in Figure 1 is illustrated with the same components having the same reference numerals from Figure 1 increased by 100.

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channel 138. A portion of the concentrate flows into each channel 136, 138.

First channel 136 directs a portion of concentrate in series through an energy recovery turbine 133 that is coupled to a common shaft 134 and a booster pump 135. Booster pump 135 is therefore driven by concentrate flow through channel 136 which drives turbine 133. The output of turbine 133 is concentrate with a substantial portion of the energy (preferably substantially all) contained therein removed.

Second channel 138 has a control valve 140 coupled in series therein to control the flow of concentrate through channel 136 and 138. Second channel 138 after control valve 140 directs concentrate between feed pump 112 and process chamber 120. In this embodiment, concentrate is preferably directed between feed pump 112 and booster pump 135.

Another known arrangement similar to Figure 1 is illustrated in Figure 4 also with reference to Figure 6 having the same components of Figure 3 illustrated with the same reference numerals. In this embodiment, first channel 136 is configured in a similar manner to that of Figure 3. Channel 138, however, is configured differently than that of Figure 3 by inserting a jet pump 142 therein. Jet pump 142 is positioned between feed pump 112 and process chamber 120. In this embodiment, jet pump 142 is preferably positioned between feed pump 112 and booster pump 135, and more specifically between

control valve 119 and booster pump 135. Jet pump 142 has a driving fluid input 144 coupled to concentrate output 124. Thus, the driving fluid of jet pump 142 is the recirculating flow whereas the pumped fluid is the feed flow from feed pump 112. By eliminating the control valve 140 from Figure 3, a portion of the energy that would have been lost is used to pressurize the combined feed and recirculation flow. Jet pump 142 has a pumped fluid input 146 used to receive feed fluid from feed pump 112. Jet pump 142 has a jet pump output 148 that directs fluid to booster pump 135.

Referring now to Figure 5, a similar arrangement to that of Figure 4 is illustrated using the same reference numerals for the same components of Figure 4. In this embodiment, jet pump 142 is positioned between booster pump 135 and process chamber 120. In this embodiment, however, the position of jet pump 142 is such that driving fluid input 144 is coupled to the output of booster pump 135 and the pressure of recirculating concentrate at pumped fluid input 146 is increased. In this embodiment, the most efficient arrangement depends on the ratio of feed flow to the recirculating flow. Generally, jet pump 142 is more efficient when the driving flow exceeds the pumped flow.

In operation, each of the embodiments of the present invention harnesses the energy from the concentrate output of the process chamber through two output channels. The first channel 136 is used to power an energy recovery turbine 133 to increase the

pressure of the feed fluid into process chamber 120.
 The second channel 138 is used to provide
 recirculation to process chamber 120 between feed
 pump 112 and process chamber 120. In the first
 5 embodiment, the second channel is coupled directly to
 the feed flow after feed pump 112 but before booster
 pump 135. Thus, the concentrate is recirculated
 through booster pump 135 and into process chamber 120
 to obtain a predetermined velocity. In the second
 10 and third embodiments, a jet pump is used to further
 increase and harness the energy from the second
 channel 138. In the second embodiment, the pump
 fluid is the fluid from feed pump 112. In the third
 embodiment, the pump fluid is the concentrate.

15 While particular embodiments of the
 invention have been shown and described, numerous
 variations and alternate embodiments will occur to
 those skilled in the art. Accordingly, it is
 intended that the invention be limited only in terms
 20 of the appended claims.

Figure 1 consists of 15 subplots, labeled (a) through (o), each showing the growth of *E. coli* O157:H7 in ground beef over a 14-day period. The y-axis for all plots is \log_{10} CFU/g, ranging from 0 to 14. The x-axis is time in days, from 0 to 14. Subplot (a) is the control, showing a steady increase in bacterial count from approximately 10^2 to 10^{11} CFU/g. Subplots (b) through (o) represent different treatments: 100% NaCl, 100% NaOH, 100% H_2O_2 , 100% Acetic acid, 100% Citric acid, 100% Lactic acid, 100% Malic acid, 100% Tartaric acid, 100% Succinic acid, 100% Fumaric acid, 100% Gluconic acid, 100% Glucuronic acid, 100% Gallic acid, and 100% Ascorbic acid, respectively. In all treatment plots, the bacterial growth is significantly inhibited compared to the control. Most treatments result in bacterial counts remaining below 10^4 CFU/g throughout the 14-day period. The growth curves for the treatments are generally lower and flatter than the control curve.

1 6. A system as recited in claim 1 further
2 comprising a second control valve coupled within said

1 7. A system as recited in claim 1 further
2 comprising a jet pump fluidically coupled to the
3 second channel to couple the high pressure outlet to
4 said feed pump outlet.

1 8. A system as recited in claim 7 wherein
2 said jet pump is coupled between said feed pump and
3 said booster pump.

1 9. A system as recited in claim 8 wherein
2 said jet pump is coupled between said booster pump
3 and said process chamber.

1 10. A reverse osmosis system comprising:
2 a reverse osmosis process chamber having a
3 first feed inlet, a first permeate outlet and a first
4 concentrate outlet;

5 a feed pump;

6 a common shaft having rotatably coupled
7 thereto a booster pump fluidically coupled between
8 said feed pump and said first feed inlet and an
9 energy recovery turbine fluidically coupled to said
10 first concentrate outlet through a first channel,
11 said energy recovery turbine driving said booster
12 pump; and

13 a second channel coupled to said first
14 concentrate outlet for directing a portion of said
15 concentrate between said booster pump and said feed
16 inlet.

12 fluidically coupling the second portion of
13 the high pressure fluid between the feed pump and the
14 process chamber.

1 17. A method as recited in claim 16
2 further comprising the steps of providing first
3 energy recovery turbine coupled to a booster pump to
4 preform the step of boosting.

1 18. A method as recited in claim 16
2 further comprising the steps of providing a jet pump
3 to preform the step of fluidically coupling.

1 19. A method as recited in claim 16
2 further comprising the steps of fluidically coupling
3 a pumped fluid input of the jet pump to the second
4 portion of high pressure fluid and fluidically
5 coupling a driving fluid input to fluid output from
6 the feed pump.

1 20. A method as recited in claim 16
2 further comprising the steps of fluidically coupling
3 a pumped fluid input of the jet pump to fluid output
4 from the feed pump and fluidically coupling a driving
5 fluid input to the second portion of high pressure
6 fluid.

FIG. 1

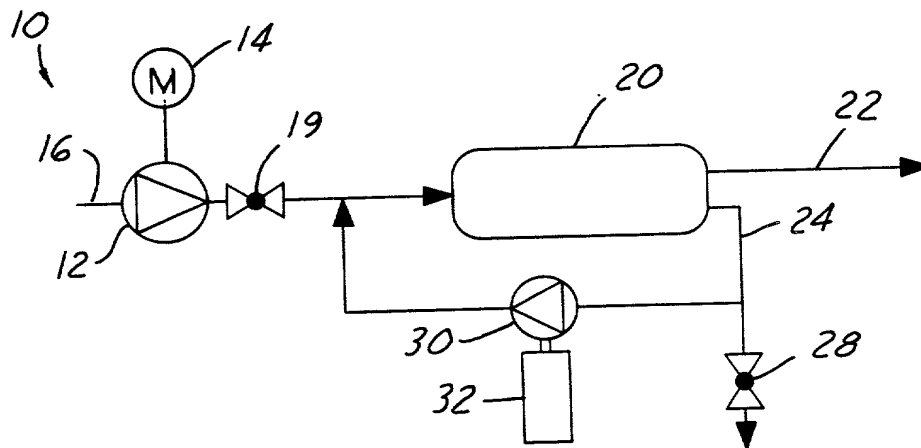


FIG. 2

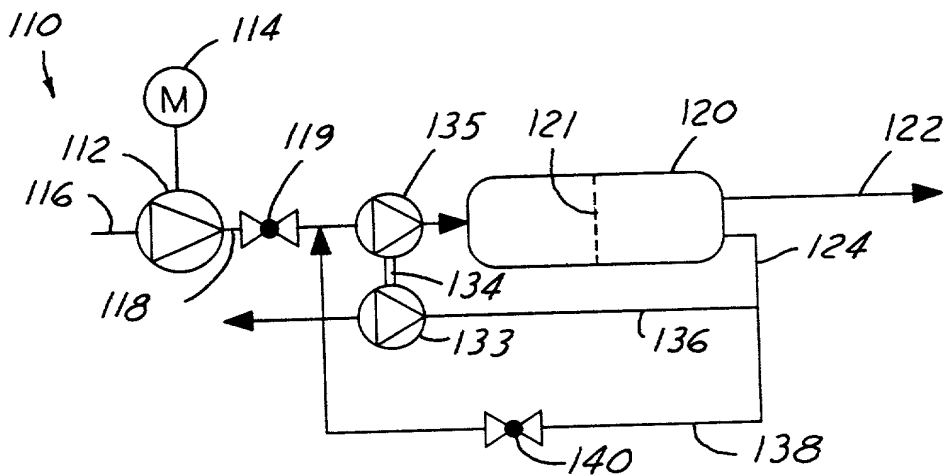


FIG. 3

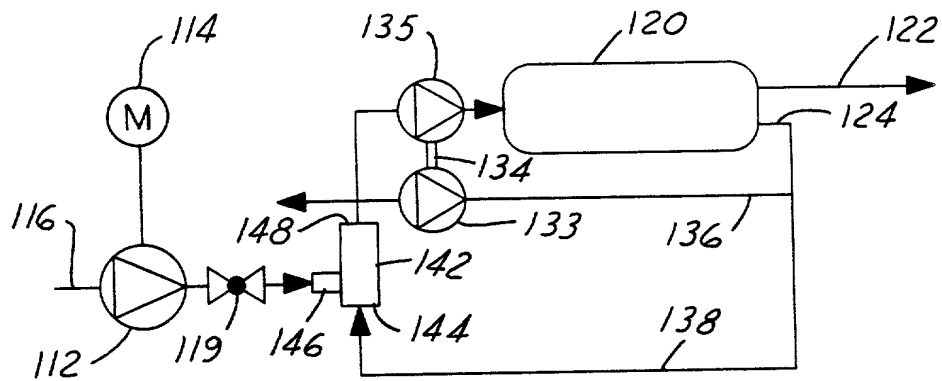


FIG. 4

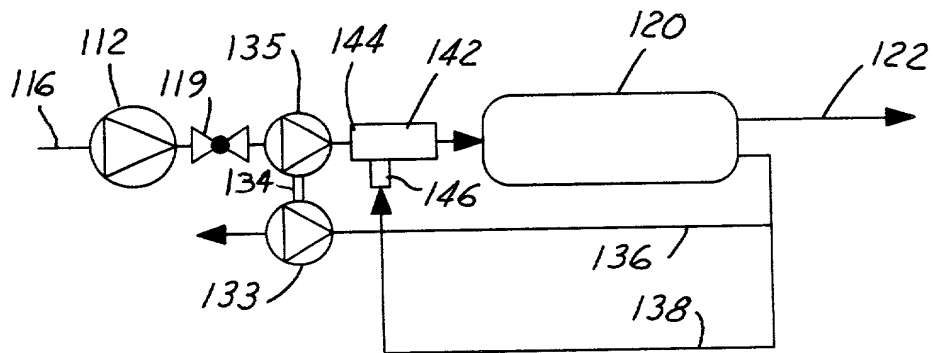


FIG. 5

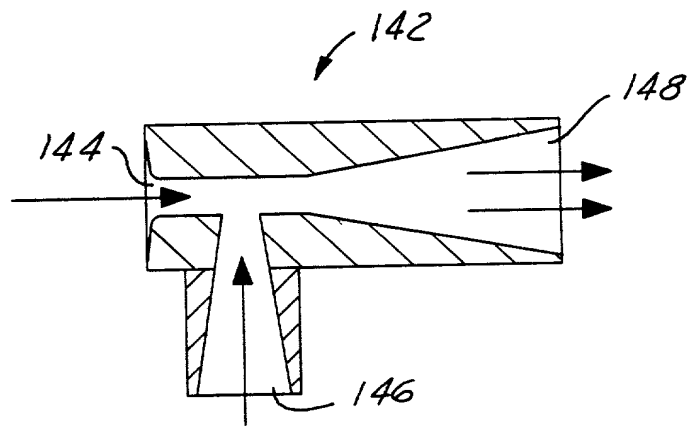


FIG. 6

**DECLARATION FOR UTILITY OR DESIGN
PATENT APPLICATION
(37 CFR 1.63)**

Attorney Docket No.: OKL 0120 PUS

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

**METHOD AND APPARATUS FOR MEMBRANE RECIRCULATION AND CONCENTRATE ENERGY
RECOVERY IN A REVERSE OSMOSIS SYSTEM**

the specification of which:

(check one) ☒ is attached hereto☐

was filed on _____; as U.S. Application Serial No. _____; and was amended on _____ (if applicable)

OR PCT International Application Number _____

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment specifically referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR § 1.56.

I hereby claim foreign priority benefits under 35 USC §119(a)-(d) or 365(b) of any foreign application(s) for patent or inventor's certificate, or 365(a) of any PCT International Application which designated at least one country other than the United States of America, listed below and have also identified below any foreign application for patent or inventor's certificate, or of any PCT International Application having a filing date before that of the application on which priority is claimed:

Prior Foreign Application(s):

Priority Claimed

Certified
Copy Attached

___ Yes ___ No

___ Yes ___ No

(Number)

(Country)

(Day/Month/Year Filed)

I hereby claim the benefit under 35 USC §120 of any United States application(s), or 365(c) of any PCT International Application designating the United States of America, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT International Application in the manner provided by the first paragraph of 35 USC §112, I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR §1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application:

Prior U.S. Application(s) OR
PCT Parent Number:

(Serial Number)

(Day/Month/Year Filed)

(Patented, pending, abandoned)

I hereby claim the benefit under 35 USC §119(e) of any United States provisional application listed below:

60/163,042

(Application Number)

11/02/99

(Day/Month/Year Filed)

As a named inventor, I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith:

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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under 18 USC 1001 and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

Full name of sole or first inventor: Eli Oklejas, Jr.

Inventor's signature: *Eli Oklejas, Jr.* Date: 31 Oct 2000

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Residence: 444 Avenue De Lafayette, Monroe, Michigan 48162